# Vapor Pressures, Critical Parameters, Boiling Points, and Triple Points of Ammonia and Trideuteroammonia

# H. W. Xiang<sup>a)</sup>

Center for Molecular Science, Institute of Chemistry, Chinese Academy of Sciences, Zhongguancun, Haidian, Beijing 100080, China

(Received 18 June 2003; accepted 9 February 2004; published online 28 October 2004)

A simple extended corresponding-states principle is used to represent the vapor pressure of ammonia and trideuteroammonia from the triple point to critical point and to describe the available experimental data along with extrapolation beyond their ranges of available experimental data. This work takes advantage of the adoption of the ITS-90 temperature scale and of the new critical parameters obtained from the extended corresponding-states principle. The vapor pressure data are described within their scatter in the entire temperature range. Comparisons with the available data show that the extended corresponding-states principle may calculate the vapor-pressure values within 0.05% -0.1% The substance-dependent characteristic parameters are given, such as critical temperature, critical density, critical pressure, acentric factor, and aspherical factor. The values of the pressures, along with their first and second derivatives as a function of temperature over the entire region from the triple point to the critical point are tabulated and recommended for scientific and practical uses. © 2004 American Institute of Physics. [DOI: 10.1063/1.1691451]

Key words: ammonia; boiling point; corresponding-states principle; critical density; critical parameters; critical pressure; critical temperature; ITS-90; thermodynamic properties; trideuteroammonia; triple point; vapor pressure.

#### Contents

1.	Introduction	1005
2.	Present Method	1006
	2.1. Vapor-Pressure Equation	1006
	2.2. The Extended Corresponding-States	
	Principle	1006
3.	Experimental Vapor-Pressure Data from the	
	Literature	1007
4.	Comparisons and Results	1011
5.	Model Uncertainty	1011
6.	Conclusions	1011
7.	Acknowledgments	1011
8.	References	1011
	List of Tables	
1.	General coefficients of the extended	
	corresponding-states principle for vapor pressure	
	in Eq. (9)	1006
2.	Experimental vapor-pressure data sources for	1000
	ammonia and trideuteroammonia	1007
3.	Critical parameters for ammonia and	1007
٠.	trideuteroammonia	1008
4.	The critical parameters, acentric factor, an	1000
٠.	aspherical factor for ammonia and	
	trideuteroammonia	1009
5.	Smoothed pressures, along with their first and	100)
٥.	second derivatives, as a function of temperature	
	for ammonia	1010
	ioi ammonia	1010

6. Smoothed pressures, along with their first and second derivatives, as a function of temperature 

### **List of Figures**

- 1. Comparison of the experimental vapor-pressure data for ammonia with values calculated from the extended corresponding-states principle..... 1008 Comparison of the experimental vapor-pressure data for trideuteroammonia with values calculated
- from the extended corresponding-states

#### 1. Introduction

Reliable data on the thermophysical properties of ammonia (NH<sub>3</sub>) and trideuteroammonia (ND<sub>3</sub>) are required for many practical applications. Since the available experimental information on the thermophysical properties of ammonia is limited, a prediction technique must be made with the aid of various theoretical methods such as the corresponding-states principle. Baehr et al. in 1976 and Haar and Gallagher in 1978 published correlations for vapor pressure from the triple point to the critical point for ammonia respectively. Tillner-Roth et al.<sup>3</sup> published a fundamental equation of state from which the vapor pressure may be calculated with some inconveniences in 1993. No vapor-pressure equation was proposed for trideuteroammonia from the triple point to the critical point.

For the description of a vapor pressure equation for ammonia, two subsequent advances are pertinent:

a)Electronic mail: hwxiang@iccas.ac.cn

1006 H. W. XIANG

- (1) A new representation of the thermodynamic temperature scale, known as ITS-90 (Preston-Thomas<sup>4</sup>); and
- (2) A simple extended corresponding-states principle that can be applied to highly nonspherical substances, as was recently developed by Xiang. <sup>5–8</sup>

This corresponding-states approach was shown to be applicable to all substances and it is applied here to ammonia.

#### 2. Present Method

# 2.1. Vapor-Pressure Equation

To represent experimental data over the entire range from the triple point to the critical temperature, the vapor-pressure curve was based upon an equation with known physical behavior and has only three substance-dependent parameters as described in the Xiang-Tan equation,<sup>9</sup>

$$\ln p_r = (a_0 + a_1 \tau^{n_1} + a_2 \tau^{n_2}) \ln T_r, \tag{1}$$

where  $\tau=1-T_r$ , the reduced temperature  $T_r=T/T_c$  with  $T_c$  being the critical temperature, and  $p_r=p/p_c$  with  $p_c$  being the critical pressure. The value of  $n_1$  is 1.89 and the values of  $n_2$  is  $3n_1$  or 5.67. The substance-dependent parameter  $a_0$  is the Riedel parameter  $n_1$  and  $n_2$  are substance-dependent parameters. The functional form presented in Eq.  $n_1$  is rewritten as

$$p_r = \exp[(a_0 + a_1 \tau^{n_1} + a_2 \tau^{n_2}) \ln T_r]$$
 (2)

and

$$p = p_c \exp[(a_0 + a_1 \tau^{n_1} + a_2 \tau^{n_2}) \ln T_r].$$
 (3)

The slope of the vapor-pressure equation is given by

$$dp/dT = \frac{d\ln p_r}{dT_r} p/T_c, \qquad (4)$$

where

$$\frac{d \ln p_r}{dT_r} = (a_0 + a_1 \tau^{n_1} + a_2 \tau^{n_2})/T_r 
- (n_1 a_1 \tau^{n_1 - 1} + n_2 a_2 \tau^{n_2 - 1}) \ln T_r.$$
(5)

At the critical point,  $d \ln p/d \ln T = \alpha_c$  is the Riedel parameter.<sup>10</sup>

The second derivative of pressure as a function of temperature is given by

$$d^{2}p/dT^{2} = \left[\frac{d^{2} \ln p_{r}}{dT_{r}^{2}} + \left(\frac{d \ln p_{r}}{dT_{r}}\right)^{2}\right] p/T_{c}^{2},\tag{6}$$

where

$$\frac{d^2 \ln p_r}{dT_r^2} = \left[n_1(n_1 - 1)a_1\tau^{n_1 - 2} + n_2(n_2 - 1)a_2\tau^{n_1 - 2}\right] \ln T_r 
- (a_0 + a_1\tau^{n_1} + a_2\tau^{n_2})/T_r^2 
- 2(n_1a_1\tau^{n_1 - 1} + n_2a_2\tau^{n_2 - 1})/T_r.$$
(7)

Equation (1) can be used to extrapolate from the precise vapor pressure measurements at modest pressures to the criti-

TABLE 1. General coefficients of the extended corresponding-states principle for vapor pressure in Eq. (9)

$a_{00}$	5.790206	$a_{10}$	6.251894	$a_{20}$	11.65859
$a_{01}$	4.888195	$a_{11}$	15.08591	$a_{21}$	46.78273
$a_{02}$	33.91196	$a_{12}$	-315.0248	$a_{22}$	-1672.179

cal point and to the triple point, provided that the critical temperature is known. When the temperature approaches the critical point, the second derivative should weakly approach infinity, which becomes significant only near several thousandth of  $\tau$ . For this case, the amplitude of the leading-order nonanalytic term in Eq. (6) is not consistent with the correct universal amplitude.

# 2.2. The Extended Corresponding-States Principle

The two-parameter corresponding-states method can only be applied accurately to spherical molecules, e.g., argon, krypton, and xenon. In order to extend the correspondingstates principle to molecular fluids, it is necessary to take into account the non-spherical nature of real molecules through the acentric factor defined by Pitzer et al., 11 which works well for a wide range of nonpolar substances but its predictive capability for polar and associating molecules is generally poor. The use of four parameters for polar fluids corresponds to an intermolecular potential function in which dispersion and dipole-dipole interaction effects are accounted for. To extend the corresponding-states principle of Pitzer et al. 11 to highly nonspherical substances, the recently developed extended corresponding-states parameter,  $\theta = (Z_c)$  $(-0.29)^2$ , was introduced to describe the deviation of the critical compression factor,  $Z_c$ , of a real nonspherical molecule from spherical molecules. 5-8 For spherical fluids  $Z_c$ = 0.29. The aspherical factor  $\theta$  is obtained from the parameters of the behavior in the critical state, which are effected by the dipole and quadrupole moments. The aspherical factor  $\theta$  reflects the physical behavior displayed by the dipole and quadrupole moments and may measure the behavior of the deviation of a highly nonspherical molecule from that of the spherical molecule argon, as is similar to the definition of the acentric factor. The relation between the critical compression factor and acentric factor,  $Z_c = 0.29 - 0.08\omega$ , <sup>11,12</sup> is only approximate for nonpolar substances and is not applicable to highly nonspherical substances. It should be noted that the aspherical factor  $\theta$  is independent for a real molecule, which significantly improves the corresponding-states behavior of polar substances. It may be deduced that the extended corresponding-states principle corresponds to adding a quadratic term  $0.0064\omega^2$  to the theory of Pitzer et al. 11 for nor-

The extended corresponding-states principle for vapor pressure reads as follows:

$$\ln p_r = \ln p_r^{(0)} + \omega \ln p_r^{(1)} + \theta \ln p_r^{(2)}, \qquad (8)$$

where the acentric factor,  $^{11}$   $\omega = -1 - \log p_r|_{T_r=0.7}$  and the aspherical factor,  $^{5-8}$   $\theta = (Z_c - 0.29)^2$  are corresponding-states

Data Temperature Pressure  $\Delta T (K)$ Author(s)  $\Delta p$  (kPa) Year points range (K) range (kPa) Ammonia Baehr et al.1 1976 16 0.008 328 - 4032325-10973 0.1(1.7+p)Beattie and Lawrence<sup>21</sup> 1930 14 303-405 1166-11298 0.2% Brill14 20 193-243 4.69 - 101.31906 Burrell and Robertson<sup>15</sup> 1915 17 159 - 2380.133 - 101.3Cragoe et al.16 150 195.4-343 1920 5.98 - 33120.01 0.02% - 0.05%Date<sup>23</sup> 1973 9 298-405 1011-11302 Gillespie et al.<sup>25</sup> 1987 4 313-394 1565-9266 0.03 0.3% Henning and Stock19 1921 5 196.6-243 6.75 - 118.8Holcomb and Outcalt<sup>27</sup> 14 0.05 3.5 1999 280 - 389558-8542 Ichihara and Uematsu<sup>26</sup> 1423-10304 0.03% 1994 12 0.01 310 - 400Keyes and Brownlee<sup>18</sup> 1918 70 273-398 435.6-9957 0.3% Overstreet and Giauque<sup>22</sup> 1937 17 195.4-241 6.075-111.3 0.05 0.00133 Zander and Thomas<sup>24</sup> 293-392 8686-9015 1979 33 0.01 0.005% Trideuteroammonia Taylor and Jungers<sup>28</sup> 1934 5 202 - 2388.3 - 83.7Jungers and Taylor<sup>29</sup> 5 1934 202 - 2388.3 - 83.7Calado et al.37 62 0.01 1992 228-259 48.2 - 222Groth et al.32 1956 31 273-294 399-835 Hart and Partington31 1943 15 212-243 17.8 - 106.5King et al.36 0.001 1989 6 198.5-243 6.22 - 105.50.005% Kirshenbaum and Urey30 1942 23 202 - 2358.3 - 72.7Streatfeild et al.35 1987 13 7.58 - 2950.01 0.1% 200 - 265Wolff and Hoepfner34 1969 13 218-273 25.3-396

TABLE 2. Experimental vapor-pressure data sources for ammonia and trideuteroammonia

parameters, here  $Z_c = p_c/R\rho_cT_c$  is the critical compression factor and  $R = 8.314\,472\,\mathrm{J\,K^{-1}\,mol^{-1}}$  is the molar gas constant recommended by Mohr and Tayler.<sup>13</sup>

To predict the vapor pressure from the corresponding-states principle, the proper reference equation must be selected which is valid from the triple point to the critical point. Equation (1) fulfills this requirement in that it can be used effectively to correlate and extrapolate the vapor-pressure behavior of simple, nonpolar, polar, hydrogen-bonding, and associating compounds. Therefore, the corresponding-states method can be used to represent vapor pressures over the entire range as<sup>5–8</sup>

$$\ln p_r^{(0)} = (a_{00} + a_{10}\tau^{n_1} + a_{20}\tau^{n_2}) \ln T_r,$$

$$\ln p_r^{(1)} = (a_{01} + a_{11}\tau^{n_1} + a_{21}\tau^{n_2}) \ln T_r,$$

$$\ln p_r^{(2)} = (a_{02} + a_{12}\tau^{n_1} + a_{22}\tau^{n_2}) \ln T_r.$$
(9)

The general coefficients  $a_{ij}$  of Eq. (9), given in Table I, were found from fitting the vapor-pressure data for argon, the weakly nonspherical molecules ethane, propane, difluoroethane, 1,1,2-tetrafluoroethane, 1,1-difluoroethane, and the highly nonspherical molecule water. The coefficients are independent of the specific substance and are expected to be universal for all classes of molecules.<sup>5–8</sup>

# 3. Experimental Vapor-Pressure Data from the Literature

Brill<sup>14</sup> determined the vapor pressure of ammonia between 193.15 K and 240 K.

Burrell and Robertson<sup>15</sup> measured the vapor pressure of ammonia from 159.8 K to 238.5 K.

Cragoe et al. 16 measured the vapor pressure of ammonia in the temperature from 195.4 K to 343 K over which temperature range 150 data points were taken in the first of two experiments, including 11 determinations for the normal boiling point. The data were taken at near uniform intervals except near the values of temperature associated with important fixed points, for which data were taken over very small intervals. Results for the boiling point were verified by a second set of measurements based on a completely independent experimental procedure. Values of temperature were measured with platinum resistance thermometers. Pressures were measured with mercury manometers and a piston gauge. The scatter of the data was in large part associated with the precision of the pressure measurements, which was about 1 part in 5000 for pressure above several atmospheres. The experimental method used for the main body of data is referred to as the static method. Certain modifications were required below 218.15 K for which region measurements were made for only three values of temperature. Throughout, the experimental values of temperature were believed to within 0.01 K. The second set of measurements was limited to determination of the normal boiling point. These measurements were based on an experimental procedure referred to as the dynamic method, which is comparatively insensitive to the presence of impurities or to the attainment of equilibrium. The mean of 17 dynamic measurements agreed with results for the determinations by the static method to within about 0.01 K and the authors suggested a value for the boil1008 H. W. XIANG

TABLE 3. Critical parameters for ammonia and trideuteroammonia

Author(s)	Year	Critical temp.	Critical pressure (kPa)	Critical density $(\rho_c/\text{kg m}^{-3})$
Ammonia				
Dewar <sup>38</sup>	1884	403.15	11652	
Vincent and Chappins <sup>39</sup>	1886	404.15	11450	
Centnerswer <sup>40</sup>	1903	405.68		
Mathias <sup>41</sup>	1904			239
Jacquerod <sup>42</sup>	1908	405.45		
Scheffer <sup>43</sup>	1910	405.25	11277	
Cardoso and Giltay44	1912	406.05	11379	
Berthoud <sup>45</sup>	1918	405.45		236
Postma <sup>46</sup>	1920	405.5	11277	
Cragoe et al.47	1922			234
Date <sup>48</sup>	1973	405.417	11318	236
Baehr <sup>1</sup>	1976	405.367	11353	234
Haar and Gallagher <sup>2</sup>	1978	405.367	11336	235
Kiselev and Rainwater <sup>49</sup>	1997	405.036	11277	234
Edison and Sengers <sup>50</sup>	1999	405.367	11336	235
This work		405.37	11345	234.3
Trideuteroammonia				
Kopper <sup>51</sup>	1992	405.2		
This work		405.2	11300	276

ing point of 239.827 K which is the average for the two methods. An overall uncertainty of 0.01 K results in an uncertainty of less than 0.1% in vapor pressure at 233.15 K. With increasing values of temperature, an uncertainty in vapor pressure becomes less than 0.05% at 273.15 K and less than 0.03% at 343.15 K. The pressure measurement indicated an uncertainty of about 0.02% for pressure above several atmospheres.

Keyes<sup>17</sup> reported vapor pressure measurements for values of temperature above 273.15 K, which corrected earlier results of Keyes and Brownlee.<sup>18</sup> The temperature scale employed was very nearly identical to ITS 1927 above 273.15 K. The data reported by Keyes and Brownlee<sup>18</sup> have very large scatter, nearly 0.3% at the higher temperatures. These measurements extend the range of the values reported by Cragoe *et al.*<sup>16</sup> to near the critical temperature. The data ob-

tained by Keyes<sup>17</sup> agree with those of Cragoe *et al.*<sup>16</sup> in their region of overlap with a maximum deviation of 0.06% and an average deviation of 0.03%, which is within the precision of either set of measurements.

Henning and Stock<sup>19</sup> reported measurements in the range from the triple point to 243 K. These data have average deviation from that of Cragoe *et al.*<sup>16</sup> of 0.3%.

McKelvey and Taylor<sup>20</sup> measured two triple-point vapor pressures and four triple-point temperatures. The spread in the four temperature measurements was less than 0.01 K with the average value of 195.493 K reported as the value of the triple-point temperature. The two vapor-pressure measurements differed by 27 Pa. The mean of the two, 6.026 kPa, was reported at the triple-point pressure. If the principal uncertainty in the pressure measurements is associated with the precision of the manometer, then a 27 Pa scatter in the data represents nearly a 0.5% error in the measured values for the triple-point pressure. The value reported for the triple-point temperature would appear to be uncertain by no more than about 0.010 K to 0.015 K.

Beattie and Lawrence<sup>21</sup> measured vapor pressure from 303.15 K to near the critical temperature, using an experimental procedure similar to that employed by Keyes.<sup>17</sup> At the lower temperature, these results are in excellent agreement with those of Cragoe *et al.*<sup>16</sup> within 0.03% at 303.15 K, however, the difference increases slightly with increasing values of temperature to just under 0.1% at 343.15 K, with an average deviation in this range of about 0.05%. The agreement is within their reported uncertainty. Above 343.15 K the data agree with those of Keyes<sup>17</sup> to within 0.1% up to 383.15 K. Differences increase to about 0.2% at 393.15 K and then uniformly to 0.8% at 405.15 K, the highest value of temperature reported, with the values of Beattie and Lawrence<sup>21</sup> being consistently higher throughout.

Overstreet and Giauque<sup>22</sup> measured the vapor pressure from the triple point to 241.6 K. Values of temperature were measured with a special gold resistance-thermometer-heater, but the primary standard was a thermocouple, which was calibrated with a hydrogen gas thermometer and compared from time to time with the gas thermometer. Such a compari-

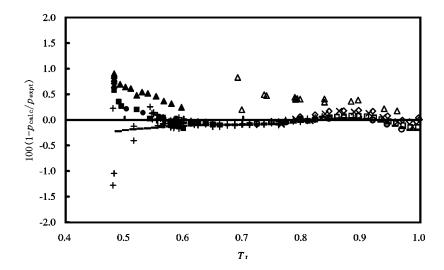


FIG. 1. Comparison of the experimental vapor-pressure data for ammonia with values calculated from the extended corresponding-states principle. ( $\square$ ) Baehr *et al.*<sup>1</sup> ( $\diamond$ ) Beattie and Lawrence<sup>21</sup>; (+) Cragoe *et al.*<sup>16</sup>; ( $\bullet$ ) Henning and Stock<sup>19</sup>; ( $\triangle$ ) Holcomb and Outcalt<sup>27</sup>; ( $\times$ ) Ichihara and Uematsu<sup>26</sup>; ( $\bullet$ ) Overstreet and Giauque<sup>22</sup>; ( $\bigcirc$ ) Zander and Thomas<sup>24</sup>; (---) Baehr *et al.*<sup>1</sup> (original).

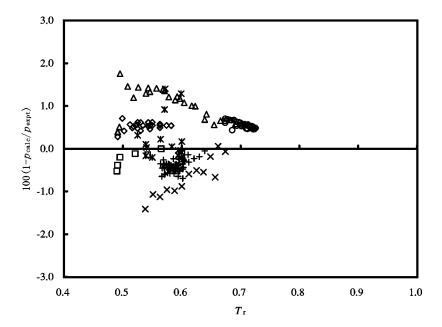


FIG. 2. Comparison of the experimental vapor-pressure data for trideuteroammonia with values calculated from the extended corresponding-states principle. (+) Calado *et al.*<sup>37</sup>; ( $\bigcirc$ ) Groth *et al.*<sup>32</sup>; (\*) Hart and Partington<sup>31</sup>; ( $\square$ ) King *et al.*<sup>36</sup>; ( $\Diamond$ ) Kirshenbaum and Urey<sup>30</sup>; ( $\triangle$ ) Streatfeild *et al.*<sup>35</sup>; ( $\times$ ) Wolff and Hoepfner.<sup>34</sup>

son was also made immediately following this experiment and the values of temperature measurements were adjusted accordingly. The precision of the gold resistance thermometer was 0.001 K, as compared with 0.01 K to 0.02 K for the primary standard, the thermocouple. Values of Overstreet and Giauque<sup>22</sup> are lower than that of Cragoe et al. 16 by about 0.04 K and 0.05 K at the triple point and the boiling point, respectively. This difference is consistent with their observations that the temperature scale can be in error by as much as 0.05 K. The pressure measurements were made with a high precision manometer, which could be read to within about 1.33 Pa. The precision achieved for pressure measurements is at least an order of magnitude greater than had been achieved in the earlier work of Cragoe et al. 16 The reported vapor-pressure value at the triple point was 6.077 kPa. The value reported by McKelvey and Taylor<sup>20</sup> was 6.026 kPa. The difference of 0.05 kPa is outside the combined precision of measurement, and is indicative of a small systematic discrepancy between the two experiments.

Date<sup>23</sup> reported measurements for the vapor pressure for the temperature range from 298.15 K to the critical temperature. The maximum differences occur at 298.15 K for which the results of Date<sup>23</sup> are about 1% too high. At 373.15 K the data reported by Date<sup>23</sup> are too low by about 0.3%. Near the

critical point the measurement by Date<sup>23</sup> tends to average the differences between those of Keyes<sup>17</sup> and of Beattie and Lawrence.<sup>21</sup>

Baehr *et al.*<sup>1</sup> reported a set of very precise data for the vapor pressure from 328.4 K to 403.6 K. These data in their region of overlap are in excellent accord with the result of Cragoe *et al.*<sup>16</sup> to within the scatter of those data. They tend to somewhat lower values than the data of Beattie and Lawrence.<sup>21</sup> Near the critical point the difference is about 0.1%. The uncertainty of the measured temperature is reported to be 0.008 K. An overall accuracy of these data is 0.05%.

Zander and Thomas<sup>24</sup> measured the vapor pressure from 293.5 K to 392.6 K. Values of the vapor pressure obtained from static measurements by using the constant volume apparatus. The reported accuracy of the measured temperature and pressure are 0.01 K and 0.005%, respectively.

Gillespie *et al.*<sup>25</sup> reported the vapor pressure of ammonia from 313.15 K to 394.3 K. The accuracy of the measured temperature and pressure are 0.03 K and 0.3%, respectively.

Ichihara and Uematsu<sup>26</sup> measured the vapor pressure from 310 K to 400 K. The pressure of the nitrogen gas was measured with two oil-operated dead-weight pressure gauges. These two pressure gauges were calibrated with a precision

TABLE 4. The critical parameters, acentric factor, and aspherical factor for ammonia and trideuteroammonia, which are obtained from the extended corresponding-states principle for vapor pressure given in Eq. (9)

	Ammonia	Trideuteroammonia		Ammonia	Trideuteroammonia
$T_c/K$	405.37	405.2	$a_0$	7.115168	7.265948
$p_c/kPa$	11345	11300	$a_1$	9.478726	9.904991
$p_c/\text{kPa}$ $\rho_c/\text{kg m}^{-3}$	234.3	276	$a_2$	20.236840	21.49400
ω	0.2568	0.287	$ ilde{ heta}$	$2.0545 \times 10^{-3}$	$2.1476 \times 10^{-3}$
$T_{ m triple}/{ m K}$	195.4	199.0	$p_{\rm triple}/{\rm kPa}$	6.0182	6.4855
$T_h/K$	239.79	242.20	$M(\text{kg kmol}^{-1})$	17.013	20.05

1010 H. W. XIANG

of 0.03%. The sample pressure was obtained by subtracting the difference between internal and external pressures of the bellows from the pressure of the nitrogen gas. This pressure difference was calibrated with an uncertainty of 0.4 kPa. The accuracy of the measured temperature and pressure is 0.01 K and 0.03%, respectively.

Holcomb and Outcalt<sup>27</sup> measured the vapor pressure from 280 K to 389.5 K. The accuracy of the measured temperature and pressure is 0.05 K and 3.5 kPa, respectively.

Taylor and Jungers<sup>28,29</sup> measured the vapor pressure of trideuteroammonia from 202 K to 238 K.

Kirshenbaum and Urey<sup>30</sup> measured the vapor pressure of trideuteroammonia from 202 K to 235 K. The accuracy of the measured temperature is 0.01 K. In the experiment, the triple-point pressures were reproducible to 3 or 4 Pa, an error of 5 Pa may exist in the pressure difference. The average error was estimated as 20 Pa.

Hart and Partington<sup>31</sup> measured the vapor pressure of trideuteroammonia from 212 K to 243 K with a large scatter of about 1%.

Groth *et al.*<sup>32</sup> measured the vapor pressure of trideuteroammonia from 273 K to 294 K.

Kiss *et al.*<sup>33</sup> reported a vapor-pressure equation of trideuteroammonia from 190 K to 243 K without experimental data.

Wolff and Hoepfner<sup>34</sup> measured the vapor pressure of trideuteroammonia from 218 K to 273 K.

Streatfeild *et al.*<sup>35</sup> measured the difference in the vapor pressure of ammonia and trideuteroammonia between 200 K and 266 K.

King et al.<sup>36</sup> measured the vapor-pressure differences of ammonia and trideuteroammonia from the triple point to 243 K. The temperature of the isotopic samples contained in separate cavities in a copper block of five-nine purity was controlled with a short-time stability, which was generally far better than 0.001 K and well within 0.001 K of each other. The absolute pressure of ammonia of natural isotopic abundance was measured with a spiral quartz gauge with a resolution of 1 Pa. Measurements of the differences in the isotopic vapor pressures were carried out with a capacitance gauge per isotopic pair.

Calado *et al.*<sup>37</sup> measured the vapor pressure between 228 K and 259 K in a twofold differential apparatus using a high-precision manometric technique. The vapor-pressure difference was monitored using capacitance sensors with a resolution of 1.3 Pa. The absolute vapor pressure of trideuteroammonia was simultaneously measured using another capacitance sensor with a resolution of 3.4 Pa. Temperatures were read with a resolution of 0.001 K and an estimated accuracy of 0.01 K.

These data resources are summarized in Table II. As pointed out by Haar and Gallagher,<sup>2</sup> there exists a considerable spread in the critical values of ammonia represented in the earlier literature as given in Table III. No experimental

TABLE 5. Smoothed pressures, along with their first and second derivatives, as a function of temperature for ammonia

T         p         dp/dT         d²p/dT²         T         p         dp/dT         d²p/dT²           (K)         (kPa)         (kPa/K)         (kPa/K²)         (K)         (kPa)         (kPa/K)         (kPa/T²)           195.40         6.0182         0.4840         3.323E - 02         303.15         1167.8         34.70         0.7827           198.15         7.4813         0.5826         3.860E - 02         308.15         1351.3         38.76         0.8407           203.15         10.922         0.8031         4.994E - 02         313.15         1555.9         43.11         0.9003           208.15         15.616         1.086         6.345E - 02         318.15         1782.9         47.76         0.9616           213.15         21.901         1.441         7.928E - 02         323.15         2034.0         52.73         1.025           218.15         30.172         1.883         9.756E - 02         328.15         2310.7         58.01         1.090           223.15         40.889         2.421         0.1184         333.15         2614.7         63.64         1.159           228.15         54.571         3.071         0.1419         338.15         2947.6								
198.15         7.4813         0.5826         3.860E-02         308.15         1351.3         38.76         0.8407           203.15         10.922         0.8031         4.994E-02         313.15         1555.9         43.11         0.9003           208.15         15.616         1.086         6.345E-02         318.15         1782.9         47.76         0.9616           213.15         21.901         1.441         7.928E-02         323.15         2034.0         52.73         1.025           218.15         30.172         1.883         9.756E-02         328.15         2310.7         58.01         1.090           223.15         40.889         2.421         0.1184         333.15         2614.7         63.64         1.159           228.15         54.571         3.071         0.1419         338.15         2947.6         69.60         1.230           233.15         71.805         3.845         0.1680         343.15         3311.3         75.94         1.304           238.15         93.246         4.756         0.1968         348.15         3707.6         82.65         1.383           239.79         101.32         5.087         0.2069         353.15         4138.5	-							
203.15         10.922         0.8031         4.994E-02         313.15         1555.9         43.11         0.9003           208.15         15.616         1.086         6.345E-02         318.15         1782.9         47.76         0.9616           213.15         21.901         1.441         7.928E-02         323.15         2034.0         52.73         1.025           218.15         30.172         1.883         9.756E-02         328.15         2310.7         58.01         1.090           223.15         40.889         2.421         0.1184         333.15         2614.7         63.64         1.159           228.15         54.571         3.071         0.1419         338.15         2947.6         69.60         1.230           233.15         71.805         3.845         0.1680         343.15         3311.3         75.94         1.304           238.15         93.246         4.756         0.1968         348.15         3707.6         82.65         1.383           239.79         101.32         5.087         0.2069         353.15         4138.5         89.78         1.467           243.15         119.61         5.817         0.2283         358.15         4606.1	195.40	6.0182	0.4840	3.323E - 02	303.15	1167.8	34.70	0.7827
208.15         15.616         1.086         6.345E-02         318.15         1782.9         47.76         0.9616           213.15         21.901         1.441         7.928E-02         323.15         2034.0         52.73         1.025           218.15         30.172         1.883         9.756E-02         328.15         2310.7         58.01         1.090           223.15         40.889         2.421         0.1184         333.15         2614.7         63.64         1.159           228.15         54.571         3.071         0.1419         338.15         2947.6         69.60         1.230           233.15         71.805         3.845         0.1680         343.15         3311.3         75.94         1.304           238.15         93.246         4.756         0.1968         348.15         3707.6         82.65         1.383           239.79         101.32         5.087         0.2069         353.15         4138.5         89.78         1.467           243.15         119.61         5.817         0.2283         358.15         4606.1         97.33         1.556           248.15         151.69         7.043         0.2624         363.15         5112.6 <t< td=""><td>198.15</td><td>7.4813</td><td>0.5826</td><td>3.860E - 02</td><td>308.15</td><td>1351.3</td><td>38.76</td><td>0.8407</td></t<>	198.15	7.4813	0.5826	3.860E - 02	308.15	1351.3	38.76	0.8407
213.15         21.901         1.441         7.928E-02         323.15         2034.0         52.73         1.025           218.15         30.172         1.883         9.756E-02         328.15         2310.7         58.01         1.090           223.15         40.889         2.421         0.1184         333.15         2614.7         63.64         1.159           228.15         54.571         3.071         0.1419         338.15         2947.6         69.60         1.230           233.15         71.805         3.845         0.1680         343.15         3311.3         75.94         1.304           238.15         93.246         4.756         0.1968         348.15         3707.6         82.65         1.383           239.79         101.32         5.087         0.2069         353.15         4138.5         89.78         1.467           243.15         119.61         5.817         0.2283         358.15         4606.1         97.33         1.556           248.15         151.69         7.043         0.2624         363.15         5112.6         105.4         1.653           253.15         190.34         8.446         0.2991         368.15         5660.5         11	203.15	10.922	0.8031	4.994E-02	313.15	1555.9	43.11	0.9003
218.15         30.172         1.883         9.756E-02         328.15         2310.7         58.01         1.090           223.15         40.889         2.421         0.1184         333.15         2614.7         63.64         1.159           228.15         54.571         3.071         0.1419         338.15         2947.6         69.60         1.230           233.15         71.805         3.845         0.1680         343.15         3311.3         75.94         1.304           238.15         93.246         4.756         0.1968         348.15         3707.6         82.65         1.383           239.79         101.32         5.087         0.2069         353.15         4138.5         89.78         1.467           243.15         119.61         5.817         0.2283         358.15         4606.1         97.33         1.556           248.15         151.69         7.043         0.2624         363.15         5112.6         105.4         1.653           253.15         190.34         8.446         0.2991         368.15         5660.5         113.9         1.758           258.15         236.47         10.04         0.3382         373.15         6252.3         122.9	208.15	15.616	1.086	6.345E - 02	318.15	1782.9	47.76	0.9616
223.15         40.889         2.421         0.1184         333.15         2614.7         63.64         1.159           228.15         54.571         3.071         0.1419         338.15         2947.6         69.60         1.230           233.15         71.805         3.845         0.1680         343.15         3311.3         75.94         1.304           238.15         93.246         4.756         0.1968         348.15         3707.6         82.65         1.383           239.79         101.32         5.087         0.2069         353.15         4138.5         89.78         1.467           243.15         119.61         5.817         0.2283         358.15         4606.1         97.33         1.556           248.15         151.69         7.043         0.2624         363.15         5112.6         105.4         1.653           253.15         190.34         8.446         0.2991         368.15         5660.5         113.9         1.758           258.15         236.47         10.04         0.3382         373.15         6252.3         122.9         1.873           263.15         291.06         11.83         0.3797         378.15         6890.9         132.6 <td>213.15</td> <td>21.901</td> <td>1.441</td> <td>7.928E - 02</td> <td>323.15</td> <td>2034.0</td> <td>52.73</td> <td>1.025</td>	213.15	21.901	1.441	7.928E - 02	323.15	2034.0	52.73	1.025
228.15         54.571         3.071         0.1419         338.15         2947.6         69.60         1.230           233.15         71.805         3.845         0.1680         343.15         3311.3         75.94         1.304           238.15         93.246         4.756         0.1968         348.15         3707.6         82.65         1.383           239.79         101.32         5.087         0.2069         353.15         4138.5         89.78         1.467           243.15         119.61         5.817         0.2283         358.15         4606.1         97.33         1.556           248.15         151.69         7.043         0.2624         363.15         5112.6         105.4         1.653           253.15         190.34         8.446         0.2991         368.15         5660.5         113.9         1.758           258.15         236.47         10.04         0.3382         373.15         6252.3         122.9         1.873           263.15         291.06         11.83         0.3797         378.15         6890.9         132.6         1.998           268.15         355.15         13.84         0.4234         383.15         7579.6         143.0 <td>218.15</td> <td>30.172</td> <td>1.883</td> <td>9.756E - 02</td> <td>328.15</td> <td>2310.7</td> <td>58.01</td> <td>1.090</td>	218.15	30.172	1.883	9.756E - 02	328.15	2310.7	58.01	1.090
233.15         71.805         3.845         0.1680         343.15         3311.3         75.94         1.304           238.15         93.246         4.756         0.1968         348.15         3707.6         82.65         1.383           239.79         101.32         5.087         0.2069         353.15         4138.5         89.78         1.467           243.15         119.61         5.817         0.2283         358.15         4606.1         97.33         1.556           248.15         151.69         7.043         0.2624         363.15         5112.6         105.4         1.653           253.15         190.34         8.446         0.2991         368.15         5660.5         113.9         1.758           258.15         236.47         10.04         0.3382         373.15         6252.3         122.9         1.873           263.15         291.06         11.83         0.3797         378.15         6890.9         132.6         1.998           268.15         355.15         13.84         0.4234         383.15         7579.6         143.0         2.138           273.15         429.82         16.07         0.4693         388.15         8321.7         154.0 <td>223.15</td> <td>40.889</td> <td>2.421</td> <td>0.1184</td> <td>333.15</td> <td>2614.7</td> <td>63.64</td> <td>1.159</td>	223.15	40.889	2.421	0.1184	333.15	2614.7	63.64	1.159
238.15         93.246         4.756         0.1968         348.15         3707.6         82.65         1.383           239.79         101.32         5.087         0.2069         353.15         4138.5         89.78         1.467           243.15         119.61         5.817         0.2283         358.15         4606.1         97.33         1.556           248.15         151.69         7.043         0.2624         363.15         5112.6         105.4         1.653           253.15         190.34         8.446         0.2991         368.15         5660.5         113.9         1.758           258.15         236.47         10.04         0.3382         373.15         6252.3         122.9         1.873           263.15         291.06         11.83         0.3797         378.15         6890.9         132.6         1.998           268.15         355.15         13.84         0.4234         383.15         7579.6         143.0         2.138           273.15         429.82         16.07         0.4693         388.15         8321.7         154.0         2.293           278.15         516.24         18.54         0.5172         393.15         9121.2         165.9 <td>228.15</td> <td>54.571</td> <td>3.071</td> <td>0.1419</td> <td>338.15</td> <td>2947.6</td> <td>69.60</td> <td>1.230</td>	228.15	54.571	3.071	0.1419	338.15	2947.6	69.60	1.230
239.79     101.32     5.087     0.2069     353.15     4138.5     89.78     1.467       243.15     119.61     5.817     0.2283     358.15     4606.1     97.33     1.556       248.15     151.69     7.043     0.2624     363.15     5112.6     105.4     1.653       253.15     190.34     8.446     0.2991     368.15     5660.5     113.9     1.758       258.15     236.47     10.04     0.3382     373.15     6252.3     122.9     1.873       263.15     291.06     11.83     0.3797     378.15     6890.9     132.6     1.998       268.15     355.15     13.84     0.4234     383.15     7579.6     143.0     2.138       273.15     429.82     16.07     0.4693     388.15     8321.7     154.0     2.293       278.15     516.24     18.54     0.5172     393.15     9121.2     165.9     2.467       283.15     615.58     21.24     0.5669     398.15     9982.4     178.7     2.663       288.15     729.11     24.21     0.6184     403.15     10910     192.6     2.889       293.15     858.09     27.43     0.6716     405.37     11345     199.1     3	233.15	71.805	3.845	0.1680	343.15	3311.3	75.94	1.304
243.15     119.61     5.817     0.2283     358.15     4606.1     97.33     1.556       248.15     151.69     7.043     0.2624     363.15     5112.6     105.4     1.653       253.15     190.34     8.446     0.2991     368.15     5660.5     113.9     1.758       258.15     236.47     10.04     0.3382     373.15     6252.3     122.9     1.873       263.15     291.06     11.83     0.3797     378.15     6890.9     132.6     1.998       268.15     355.15     13.84     0.4234     383.15     7579.6     143.0     2.138       273.15     429.82     16.07     0.4693     388.15     8321.7     154.0     2.293       278.15     516.24     18.54     0.5172     393.15     9121.2     165.9     2.467       283.15     615.58     21.24     0.5669     398.15     9982.4     178.7     2.663       288.15     729.11     24.21     0.6184     403.15     10910     192.6     2.889       293.15     858.09     27.43     0.6716     405.37     11345     199.1     3.004	238.15	93.246	4.756	0.1968	348.15	3707.6	82.65	1.383
248.15     151.69     7.043     0.2624     363.15     5112.6     105.4     1.653       253.15     190.34     8.446     0.2991     368.15     5660.5     113.9     1.758       258.15     236.47     10.04     0.3382     373.15     6252.3     122.9     1.873       263.15     291.06     11.83     0.3797     378.15     6890.9     132.6     1.998       268.15     355.15     13.84     0.4234     383.15     7579.6     143.0     2.138       273.15     429.82     16.07     0.4693     388.15     8321.7     154.0     2.293       278.15     516.24     18.54     0.5172     393.15     9121.2     165.9     2.467       283.15     615.58     21.24     0.5669     398.15     9982.4     178.7     2.663       288.15     729.11     24.21     0.6184     403.15     10910     192.6     2.889       293.15     858.09     27.43     0.6716     405.37     11345     199.1     3.004	239.79	101.32	5.087	0.2069	353.15	4138.5	89.78	1.467
253.15     190.34     8.446     0.2991     368.15     5660.5     113.9     1.758       258.15     236.47     10.04     0.3382     373.15     6252.3     122.9     1.873       263.15     291.06     11.83     0.3797     378.15     6890.9     132.6     1.998       268.15     355.15     13.84     0.4234     383.15     7579.6     143.0     2.138       273.15     429.82     16.07     0.4693     388.15     8321.7     154.0     2.293       278.15     516.24     18.54     0.5172     393.15     9121.2     165.9     2.467       283.15     615.58     21.24     0.5669     398.15     9982.4     178.7     2.663       288.15     729.11     24.21     0.6184     403.15     10910     192.6     2.889       293.15     858.09     27.43     0.6716     405.37     11345     199.1     3.004	243.15	119.61	5.817	0.2283	358.15	4606.1	97.33	1.556
258.15     236.47     10.04     0.3382     373.15     6252.3     122.9     1.873       263.15     291.06     11.83     0.3797     378.15     6890.9     132.6     1.998       268.15     355.15     13.84     0.4234     383.15     7579.6     143.0     2.138       273.15     429.82     16.07     0.4693     388.15     8321.7     154.0     2.293       278.15     516.24     18.54     0.5172     393.15     9121.2     165.9     2.467       283.15     615.58     21.24     0.5669     398.15     9982.4     178.7     2.663       288.15     729.11     24.21     0.6184     403.15     10910     192.6     2.889       293.15     858.09     27.43     0.6716     405.37     11345     199.1     3.004	248.15	151.69	7.043	0.2624	363.15	5112.6	105.4	1.653
263.15     291.06     11.83     0.3797     378.15     6890.9     132.6     1.998       268.15     355.15     13.84     0.4234     383.15     7579.6     143.0     2.138       273.15     429.82     16.07     0.4693     388.15     8321.7     154.0     2.293       278.15     516.24     18.54     0.5172     393.15     9121.2     165.9     2.467       283.15     615.58     21.24     0.5669     398.15     9982.4     178.7     2.663       288.15     729.11     24.21     0.6184     403.15     10910     192.6     2.889       293.15     858.09     27.43     0.6716     405.37     11345     199.1     3.004	253.15	190.34	8.446	0.2991	368.15	5660.5	113.9	1.758
268.15     355.15     13.84     0.4234     383.15     7579.6     143.0     2.138       273.15     429.82     16.07     0.4693     388.15     8321.7     154.0     2.293       278.15     516.24     18.54     0.5172     393.15     9121.2     165.9     2.467       283.15     615.58     21.24     0.5669     398.15     9982.4     178.7     2.663       288.15     729.11     24.21     0.6184     403.15     10910     192.6     2.889       293.15     858.09     27.43     0.6716     405.37     11345     199.1     3.004	258.15	236.47	10.04	0.3382	373.15	6252.3	122.9	1.873
273.15     429.82     16.07     0.4693     388.15     8321.7     154.0     2.293       278.15     516.24     18.54     0.5172     393.15     9121.2     165.9     2.467       283.15     615.58     21.24     0.5669     398.15     9982.4     178.7     2.663       288.15     729.11     24.21     0.6184     403.15     10910     192.6     2.889       293.15     858.09     27.43     0.6716     405.37     11345     199.1     3.004	263.15	291.06	11.83	0.3797	378.15	6890.9	132.6	1.998
278.15     516.24     18.54     0.5172     393.15     9121.2     165.9     2.467       283.15     615.58     21.24     0.5669     398.15     9982.4     178.7     2.663       288.15     729.11     24.21     0.6184     403.15     10910     192.6     2.889       293.15     858.09     27.43     0.6716     405.37     11345     199.1     3.004	268.15	355.15	13.84	0.4234	383.15	7579.6	143.0	2.138
283.15     615.58     21.24     0.5669     398.15     9982.4     178.7     2.663       288.15     729.11     24.21     0.6184     403.15     10910     192.6     2.889       293.15     858.09     27.43     0.6716     405.37     11345     199.1     3.004	273.15	429.82	16.07	0.4693	388.15	8321.7	154.0	2.293
288.15     729.11     24.21     0.6184     403.15     10910     192.6     2.889       293.15     858.09     27.43     0.6716     405.37     11345     199.1     3.004	278.15	516.24	18.54	0.5172	393.15	9121.2	165.9	2.467
293.15 858.09 27.43 0.6716 405.37 11345 199.1 3.004	283.15	615.58	21.24	0.5669	398.15	9982.4	178.7	2.663
	288.15	729.11	24.21	0.6184	403.15	10910	192.6	2.889
298.15 1003.9 30.93 0.7263	293.15	858.09	27.43	0.6716	405.37	11345	199.1	3.004
	298.15	1003.9	30.93	0.7263				

data in the high-temperature region and for the critical pressure and critical density of trideuteroammonia have been reported yet. All literature data were converted to ITS-90, the temperature scale used throughout this work.

TABLE 6. Smoothed pressures, along with their first and second derivatives, as a function of temperature for trideuteroammonia

T (K)	p (kPa)	dp/dT (kPa/K)	$\frac{d^2p/dT^2}{(\text{kPa/K}^2)}$	T (K)	p (kPa)	dp/dT (kPa/K)	$\frac{d^2p/dT^2}{(\text{kPa/K}^2)}$
199.00	6.4855	0.5180	3.532E - 02	303.15	1107.3	33.75	0.7846
203.15	8.9636	0.6824	4.413E-02	308.15	1286.1	37.82	0.8452
208.15	12.977	0.9335	5.671E - 02	313.15	1486.0	42.20	0.9076
213.15	18.413	1.253	7.161E - 02	318.15	1708.6	46.90	0.9721
218.15	25.645	1.654	8.900E-02	323.15	1955.5	51.93	1.039
223.15	35.107	2.148	0.1090	328.15	2228.4	57.29	1.108
228.15	47.299	2.748	0.1317	333.15	2529.0	63.01	1.179
233.15	62.791	3.469	0.1572	338.15	2859.1	69.09	1.255
238.15	82.218	4.325	0.1855	343.15	3220.6	75.56	1.333
242.20	101.32	5.127	0.2106	348.15	3615.4	82.43	1.417
243.15	106.29	5.330	0.2167	353.15	4045.6	89.73	1.505
248.15	135.79	6.497	0.2507	358.15	4513.5	97.50	1.600
253.15	171.55	7.841	0.2874	363.15	5021.4	105.8	1.703
258.15	214.51	9.375	0.3268	368.15	5571.9	114.5	1.814
263.15	265.64	11.11	0.3688	373.15	6167.8	123.9	1.936
268.15	326.00	13.07	0.4133	378.15	6812.0	133.9	2.070
273.15	396.69	15.25	0.4601	383.15	7508.1	144.6	2.218
278.15	478.90	17.67	0.5092	388.15	8259.6	156.1	2.383
283.15	573.83	20.35	0.5605	393.15	9070.8	168.5	2.568
288.15	682.79	23.28	0.6137	398.15	9946.2	181.8	2.778
293.15	807.08	26.49	0.6688	403.15	10891	196.3	3.019
298.15	948.11	29.97	0.7258	405.2	11300	202.6	3.133

# 4. Comparisons and Results

The experimental data are compared with values calculated from the present method as shown in Figs. 1 and 2. Additional experimental data in the high temperature region is needed for trideuteroammonia. The critical parameters, acentric factor, aspherical factor, normal-boiling-point and triple-point temperatures are listed in Table IV. Smoothed pressures, along with their first and second derivatives, as a function of temperature in the range between the triple point and the critical point for ammonia and trideuteroammonia from the present method are presented in Tables V and VI.

# 5. Model Uncertainty

Generally speaking, the uncertainty of vapor pressures determined by the extended corresponding-states method is within the experimental uncertainties for the most accurate data (refer to the extensive application of the present method in previous works<sup>5–8</sup>). The average deviations between the vapor pressures obtained from the present method, Eq. (9), and the experimental data are shown in Figs. 1 and 2. The uncertainties of the present method were verified to be approximately 0.05%–0.1% in the vapor pressure for substances whose have accurate experimental data, even in a limited range. The uncertainties are less than 0.1% for the first derivative and are several percentages for the second derivative according to our mathematical experience.

#### 6. Conclusions

All data included in the previous vapor pressure equation were converted to the ITS-90 temperature scale. The vapor-pressure values obtained by the extended corresponding-states principle are in agreement with the published experimental data within their uncertainties. The uncertainty in the vapor pressure is estimated at 0.05%-0.1% since the extended corresponding-states principle is used in the present method. The previous vapor-pressure equations for ammonia and trideuteroammonia do not adequately describe these data because it was based on the IPTS-68 temperature scale and in a limited range. An advantage of the present method is that it allows accurate values to be calculated directly without requiring any temperature conversion.

## 7. Acknowledgments

The financial support from the Foundations of the Chinese Academy of Sciences, of Departments of Personnel and of Education, and the Natural Science Foundation of China is gratefully appreciated. The author would like to thank some people, in particular, Dr. Marcia L. Huber, Dr. Eric W. Lemmon, and Dr. Joseph W. Magee at NIST for making productive comments. The author thanks Editor Malcolm W. Chase and Linda Diane Decker for valuable revisions.

#### 8. References

- <sup>1</sup>H. D. Baehr, H. Garnjost, and R. Pollak, J. Chem. Thermodyn. **8**, 113 (1976).
- <sup>2</sup>L. Haar and J. S. Gallagher, J. Phys. Chem. Ref. Data 7, 635 (1978).
- <sup>3</sup>R. Tillner-Roth, F. Harms-Watzenberg, and H. D. Baehr, DKV-Tagungsbericht **20**, 167 (1993).
- <sup>4</sup>H. Preston-Thomas, Metrologia 27, 3 (1990).
- <sup>5</sup>H. W. Xiang, Int. J. Thermophys. **22**, 919 (2001).
- <sup>6</sup>H. W. Xiang, J. Phys. Chem. Ref. Data **30**, 1161 (2001).
- <sup>7</sup>H. W. Xiang, Chem. Eng. Sci. **57**, 1439 (2002).
- <sup>8</sup>H. W. Xiang, J. Phys. Chem. Ref. Data **32**, 1707 (2003).
- <sup>9</sup> H. W. Xiang and L. C. Tan, Int. J. Thermophys. 15, 711 (1994).
- <sup>10</sup>L. Riedel, Chem.-Ing.-Tech. **26**, 83 (1954).
- <sup>11</sup> K. S. Pitzer, D. Z. Lippmann, R. F. Curl, C. M. Huggins, and D. E. Petersen, J. Am. Chem. Soc. **77**, 3433 (1955).
- <sup>12</sup> R. C. Reid, J. M. Prausnitz, and B. E. Poling, *The Properties of Gases and Liquids*, 4th ed. (McGraw-Hill, New York, 1987).
- <sup>13</sup>P. J. Mohr and B. N. Taylor, J. Phys. Chem. Ref. Data **28**, 1713 (1999).
- <sup>14</sup>O. Brill, Ann. Phys. (Leipzig) **21**, 170 (1906).
- <sup>15</sup>G. A. Burrell and I. W. Robertson, J. Am. Chem. Soc. 37, 2482 (1915).
- <sup>16</sup>C. S. Cragoe, C. H. Meyers, and C. S. Taylor, J. Am. Chem. Soc. **42**, 206 (1920); Sci. Pap. Bur. Stands. **16**, 1 (1920).
- <sup>17</sup>F. G. Keyes, AHRAE J. **7**, 371 (1921).
- <sup>18</sup>F. G. Keyes and R. B. Brownlee, J. Am. Chem. Soc. **40**, 25 (1918).
- <sup>19</sup> F. Henning and A. Stock, Z. Phys. **4**, 226 (1921).
- <sup>20</sup>E. C. McKelvey, and C. S. Taylor, Sci. Pap. Bur. Stand. 18, 655 (1923).
- <sup>21</sup> J. A. Beattie, and C. K. Lawrence, J. Am. Chem. Soc. **52**, 6 (1930).
- <sup>22</sup>R. Overstreet and W. F. Giauque, J. Am. Chem. Soc. **59**, 254 (1937).
- <sup>23</sup> K. Date, Rev. Phys. Chem. Jpn. **43**, 1 (1973).
- <sup>24</sup>M. Zander and W. Thomas, J. Chem. Eng. Data **24**, 1 (1979).
- <sup>25</sup> P. C. Gillespie, W. V. Wilding, and G. M. Wilson, AIChE Symp. Ser. 83(256), 97 (1987).
- <sup>26</sup>T. Ichihara and M. Uematsu, J. Chem. Thermodyn. **26**, 1129 (1994).
- $^{27}\,\text{C.}$  D. Holcomb and S. L. Outcalt, Fluid Phase Equilib. 164, 97 (1999).
- <sup>28</sup>H. S. Taylor and J. C. Jungers, J. Am. Chem. Soc. **55**, 5057 (1933).
- <sup>29</sup> J. C. Jungers and H. S. Taylor, J. Chem. Phys. **2**, 373 (1934).
- <sup>30</sup>I. Kirshenbaum and H. C. Urey, J. Chem. Phys. **10**, 706 (1942).
- <sup>31</sup> A. B. Hart and J. R. Partington, J. Chem. Soc. **1943**, 104 (1943).
- <sup>32</sup> W. Groth, H. Ihle, and A. Murrenhoff, Angew. Chem. **68**, 605 (1956).
- <sup>33</sup>I. Kiss, L. Matus, and I. Opauszky, Kernenergie 5, 329 (1962).
- <sup>34</sup>H. Wolff and A. Hoepfner, Ber. Bunsenges. Phys. Chem. **73**, 480 (1969).
- <sup>35</sup> M. H. Streatfeild, C. Henderson, L. A. K. Staveley, A. G. M. Ferreira, I. M. A. Fonseca, and L. Q. Lobo, J. Chem. Thermodyn. 19, 1163 (1987).
- <sup>36</sup>T.-V. King, T. Oi, A. Popowicz, K. Heinzinger, and T. Ishida, Z. Naturforsch., A: Phys. Sci. 44A, 359 (1989).
- 37 J. C. G. Calado, J. N. C. Lopes, and L. P. N. Rebelo, J. Chem. Thermodyn.
   24, 993 (1992).
- <sup>38</sup> J. Dewar, Philos. Mag. **18**, 210 (1884).
- <sup>39</sup>C. Vincent and J. Chappuis, J. Phys. Ser. 2 5, 58 (1886).
- <sup>40</sup>M. Centnerswer, Z. Phys. Chem., Stoechiom. Verwandtschaftsl. **46**, 456 (1903).
- <sup>41</sup> M. E. Mathias, Le Point Critique des Corps Purs. (Gauthier-Villars, Paris, 1904).
- <sup>42</sup> A. Jacquerod, Mem. Soc. Phys. Geneve **35**, 686 (1908).
- <sup>43</sup> F. E. C. Scheffer, Z. Phys. Chem., Stoechiom. Verwandtschaftsl. **71**, 695 (1910).
- <sup>44</sup>M. E. Cardoso and A. Giltay, J. Chim. Phys. Phys.-Chim. Biol. **10**, 514 (1912).
- <sup>45</sup> A. Berthoud, Helv. Chim. Acta **1**, 84 (1918).
- <sup>46</sup>S. Postma, Recl. Trav. Chim. Pays-Bas **89**, 515 (1920).
- <sup>47</sup>C. S. Cragoe, E. C. McKelvey, and G. F. O'Connor, Sci. Pap. Bur. Stands. 18, 707 (1922).
- <sup>48</sup> K. Date, Rev. Phys. Chem. Jpn. **43**, 17 (1973).
- <sup>49</sup>S. B. Kiselev and J. C. Rainwater, Fluid Phase Equilib. **141**, 129 (1997).
- <sup>50</sup>T. A. Edison and J. V. Sengers, Int. J. Refrig. **22**, 365 (1999).
- <sup>51</sup> H. Kopper, Z. Phys. Chem. Abt. A **175A**, 469 (1936).